

# FM.1 Fluid Mechanics, Simplified Analyses

## Conservation principles, *Eulerian* viewpoint

$$DM = \frac{\partial}{\partial t} \int_{CV} \rho d\tau + \oint_{CS} \rho \mathbf{V} \cdot \hat{\mathbf{n}} d\sigma = 0$$

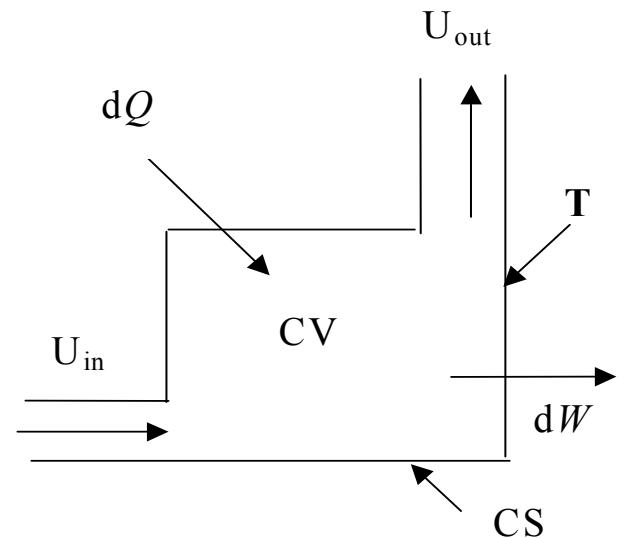
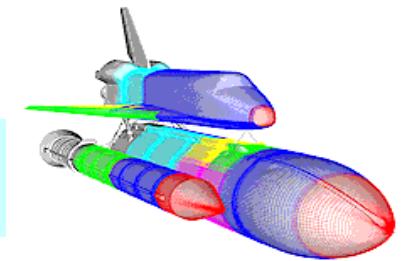
$$DP \Rightarrow \frac{\partial}{\partial t} \int_{CV} \rho \mathbf{V} d\tau + \oint_{CS} \mathbf{V} \rho \mathbf{V} \cdot \hat{\mathbf{n}} d\sigma = \int_{CV} \rho \mathbf{B} d\tau + \int_{CS} \mathbf{T} d\sigma$$

$$DE \Rightarrow \frac{\partial}{\partial t} \int_{CV} \rho e d\tau + \oint_{CS} (e + p/\rho) \rho \mathbf{V} \cdot \hat{\mathbf{n}} d\sigma = \int_{CV} s d\tau + \oint_{CS} (W - \mathbf{q} \cdot \hat{\mathbf{n}}) d\sigma$$

## Control volume, uni-directional flow

$DM, DE \Rightarrow$  algebraic equations  
 $\text{physics} \Rightarrow$  heat added, work done  
 $DP \Rightarrow$  reaction force  $\mathbf{T}$

data: velocity in, heat added, fluid properties  
output: velocity out, work done, reaction force



# FM.2 Fluid Mechanics, Constitutive Closure Models

## Conservation principles, arbitrary Eulerian CV

$$D M : \frac{\partial \rho}{\partial t} + \nabla \cdot \rho \mathbf{V} = 0$$

$$D \mathbf{P} : \frac{\partial \rho \mathbf{V}}{\partial t} + \nabla \cdot \rho \mathbf{V} \mathbf{V} = \rho \mathbf{g} + \nabla \cdot \mathbf{T}$$

$$D E : \frac{\partial \rho e}{\partial t} + \nabla \cdot (\rho e + p) \mathbf{V} = s - \nabla \cdot \mathbf{q}$$

## Constitutive closure models $\Rightarrow$ Navier-Stokes equations

Stokes viscosity model

$$\mathbf{T} \equiv -p \mathbf{I} + \mu \cdot \nabla \mathbf{V} - \frac{2\lambda}{3} (\nabla \cdot \mathbf{V}) \delta$$

Fourier conduction model

$$\mathbf{q} = -k \nabla T$$

perfect gas, internal energy

$$p = \rho R T, \quad e = c_v T, \quad c = \sqrt{\gamma R T}$$

where:  $\mu, \lambda, k, R, c_v$  are fluid properties (data)

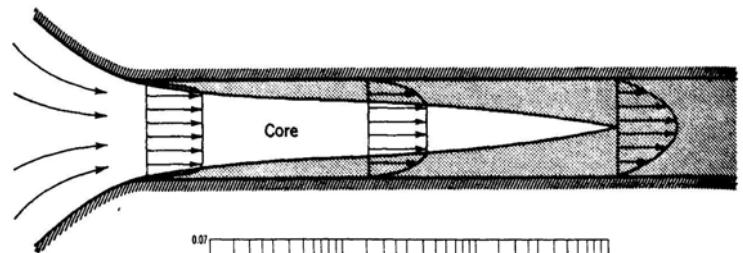
# FM.3 Fluid Mechanics, Navier-Stokes Equations

## One-dimensional simplifications

textbook pipe flow

physics – laminar,  $DE = 0$

**DP**  $\Rightarrow$  ordinary differential equations



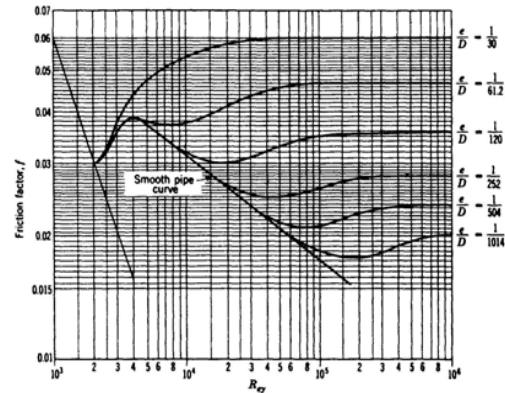
practical pipe flow

physics - turbulent flow

**DP**  $\Rightarrow$  data correlations (Re,  $\varepsilon/D$ )

concepts – similitude, roughness

**DM, DE**  $\Rightarrow$  piping networks, pumping



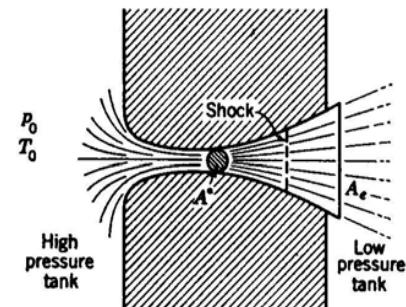
compressible flow

physics – isentropic ( $\mu = 0 = k$ )

– perfect gas ( $\gamma, R$ )

**DM, DE**  $\Rightarrow$  exponential algebraic equations  
concepts – sonic throat, shock

**DP**  $\Rightarrow$  reaction force



# FM.4 Navier-Stokes Equations, non-Dimensional

non-D, incompressible laminar flow + heat transfer

$$DM : \nabla \cdot \mathbf{u} = 0$$

$$DP : \frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{u} + \nabla P - \frac{1}{Re} \nabla^2 \mathbf{u} - \frac{Gr}{Re^2} \Theta \hat{\mathbf{g}} = 0$$

$$DE : \frac{\partial \Theta}{\partial t} + (\mathbf{u} \cdot \nabla) \Theta - \frac{1}{Re \Pr} \nabla^2 \Theta - s = 0$$

on  $\Omega \subset \mathfrak{R}^n$  + BCs + IC

closure models, non-D groups

closure models:

$$\rho g \Rightarrow Gr Re^{-2} \Theta \hat{\mathbf{g}}$$

$$T \Rightarrow Re^{-1}$$

$$q \Rightarrow (Re Pr)^{-1}$$

$$BCs \Rightarrow Nu$$

non-D variables:

$$\Theta = (T - T_{min}) / \Delta T$$

$$\mathbf{u} = \mathbf{V} / U_\infty$$

$$P = p / \rho_0 U_\infty^2$$

$$Grashoff = Gr = \rho_0^2 \beta g \Delta T L^3 / \mu^2$$

$$Reynolds = Re = \rho_0 U L / \mu$$

$$Prandtl = Pr = c_p \mu / k$$

$$Nusselt = Nu = h L / k$$

$$Rayleigh = Ra = \frac{\beta g k}{\rho c_p \mu U^2} (\Delta T)$$

# FM.5 Navier-Stokes, Aerodynamics Simplification

## Characteristics of aerodynamic flows

aerodynamic shapes

flowfield is uni-directional

farfield is undistributed

large Reynolds number,  $Re/L > 10^6$

viscous effects strictly local



## Conservation principle simplifications

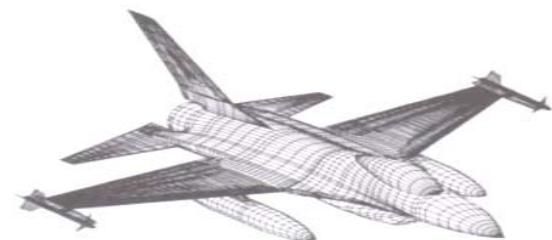
farfield described by potential flow  $\Rightarrow \mathbf{u} = -\nabla\phi$

$$DM: \nabla \cdot \rho \mathbf{u} \Rightarrow -\nabla \cdot \rho \nabla \phi = 0$$

$$\int D \mathbf{P} \cdot d\Psi \Rightarrow p(\mathbf{x}) = p_{\infty} - \frac{1}{2} \rho \mathbf{u} \cdot \mathbf{u}$$

Bernoulli pressure

nearfield  $DM + D\mathbf{P}$  can be Re-ordered  
 $\Rightarrow$  boundary layer form of N-S



# FM.6 Aerodynamics – Potential Flow

## Inviscid, irrotational steady flow

subsonic – transonic – supersonic:  $\text{Mach} \equiv M = U/a$ ,  $a = \sqrt{\gamma RT} = \sqrt{U_\infty / (\gamma RT)}$

$$M_a < 0.3 : DM = \nabla \cdot \mathbf{u} \Rightarrow -\nabla^2 \phi = 0$$

$$M_a \approx 1 : DM = \nabla \cdot \rho \mathbf{u} \Rightarrow (1 - M_\infty^2) \frac{\partial^2 \phi}{\partial x^2} + \frac{\partial^2 \phi}{\partial y^2} - M_\infty^2 \left[ \frac{1+\gamma}{U_\infty} \right] \frac{\partial \phi}{\partial x} \frac{\partial^2 \phi}{\partial x^2} = 0$$

$$M_a > 1 : DM = \nabla \cdot \rho \mathbf{u} \Rightarrow (1 - M_x^2) \frac{\partial^2 \phi}{\partial x^2} + (1 + M_y^2) \frac{\partial^2 \phi}{\partial y^2} - \frac{2}{a^2} \frac{\partial \phi}{\partial x} \frac{\partial \phi}{\partial y} \frac{\partial^2 \phi}{\partial x \partial y} = 0$$

Mach  $\leq 0.3$



Mach  $\approx 1$



Mach  $> 1$

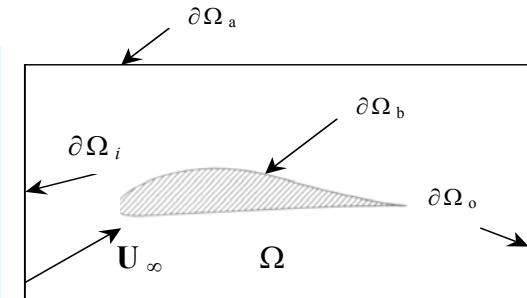


# FM.7 Subsonic Potential Flow

## n - D subsonic aerodynamics

**DM:**

$$\begin{aligned} L(\phi) &= -\nabla^2 \phi = 0 & , \text{on } \Omega \subset \Re^n \\ \ell(\phi) &= \mathbf{u} \cdot \hat{\mathbf{n}} = -\hat{\mathbf{n}} \cdot \nabla \phi = 0 & , \text{on } \partial\Omega_{\text{body}} \\ &= \mathbf{U}_\infty \cdot \hat{\mathbf{n}} & , \text{on } \partial\Omega_{\text{inflow}} \\ \phi(\mathbf{x}_b) &= 0 & , \text{on } \partial\Omega_{\text{outflow}} \end{aligned}$$

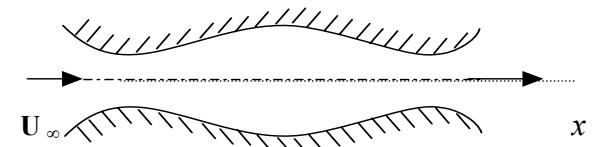


$$GWS^h = S_e \{WS\}_e = 0, \quad \{WS\}_e = (\ )(\ )( \ }(-1)[M2KK]\{PHI\} + BCs$$

## quasi-one dimensional ducted flow

**DM:**

$$L(\phi) = -A(x) \frac{d^2\phi}{dx^2} - \frac{dA}{dx} \frac{d\phi}{dx} = 0$$



$$\begin{aligned} \{WS(\phi^h)\}_e &= (\ )( \ }(\{AREA\})(-1)[A3011]\{PHI\} \\ &+ (\ )( \ }(\{AREA\})(-1)[A3101]\{PHI\} \\ &+ (-)( \ }(\{AREA\})(-1)[A3101]\{PHI\} \\ &+ (UDOTN)( \ }(\{AREA\})( \ }(\{ONE\})\{ \ }) \end{aligned}$$

**DE:**

$$L(p) = p - p_\infty + \frac{1}{2}\rho(d\phi/dx)^2$$

$$\begin{aligned} \{WS(P)\}_e &= (\ )( \ }(\{ \ })(1)[A200]\{P\} + (-)( \ }(\{ \ })(1)[A200]\{P_{inf}\} \\ &+ (1/2, RHO)( \ }(\{PHI\})(-1)[A3101]\{PHI\} \end{aligned}$$

# FM.8 Aerodynamics, Weak Interaction Theory

## Farfield, subsonic-transonic potential flow assumption

DM:

$$L(\phi) = (1 - M_\infty^2) \frac{\partial^2 \phi}{\partial x^2} + \frac{\partial^2 \phi}{\partial y^2} + \frac{\partial^2 \phi}{\partial z^2} = 0$$

$$\ell(t) = \hat{\mathbf{n}} \cdot \nabla \phi - U_\infty \hat{\mathbf{i}} \cdot \hat{\mathbf{n}} = 0$$

DE:

$$p(\mathbf{x}_\delta) = p_\infty - \rho \nabla \phi \cdot \nabla \phi / 2$$

## Nearfield, boundary layers wash aerosurfaces

viscous, turbulent effects dominate

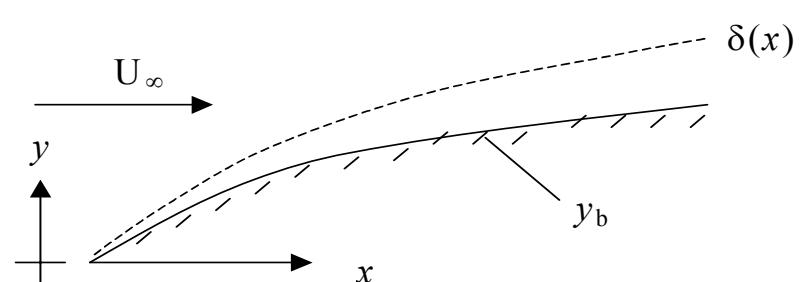
DM:

$$\nabla \cdot \mathbf{u} = 0$$

DP:

$$\mathbf{u} \cdot \nabla \mathbf{u} = \frac{-1}{\rho_0} \nabla p + \nabla T$$

in the region  $y_b(x) \leq y(x) \leq \delta(x)$



$\delta(x) \equiv$  boundary layer thickness

$T$  = viscous + turbulent effects

# FM.9 Aerodynamics, Boundary Layer Flow

## Reynolds ordering of Navier-Stokes, subsonic, $n = 2$

known scales:  $U_\infty, L, \delta(x)$

non-D ordering:  $u/U_\infty \approx O(1), x/L \approx O(1), \delta/L \ll O(1)$

DM:

$$\nabla \cdot \mathbf{u} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$
$$\Rightarrow O(1/1) + O(v/\delta) = 0, \text{ hence, } v/U_\infty \approx O(\delta)$$

DP:

$$\mathbf{u} \cdot \nabla \mathbf{u} + Eu \nabla p - Re^{-1} \nabla^2 \mathbf{u} = 0$$

$$\hat{\mathbf{i}} \Rightarrow O(1 \cdot 1/1) + O(\delta \cdot 1/\delta) + Eu O(p/1) - Re^{-1} O(1/1 \cdot 1 + 1/\delta \cdot \delta) = 0$$

keeping  $O(1) \Rightarrow Eu \partial p / \partial x \Rightarrow O(1)$ ,  $Re^{-1} \Rightarrow O(\delta^2)$ ,  $\frac{\partial^2 u}{\partial x^2} \Rightarrow O(\delta^2)$

$$\hat{\mathbf{j}} \Rightarrow O(1 \cdot \delta/1) + O(\delta \cdot \delta/\delta) + Eu O(1/\delta) - Re^{-1} O(\delta/1 \cdot 1 + \delta/\delta \cdot \delta) = 0$$

everything  $O(\delta) \Rightarrow$  hence  $Eu \partial p / \partial y = O(\delta)$ , then  $p(x, y) \Rightarrow p(x)$

recall:

$$Re = \rho_\infty U_\infty L / \mu_\infty$$

$$Eu = p_\infty / \rho_\infty U_\infty^2$$

# FM.10 Boundary Layer Form of Navier-Stokes

**Summary, Reynolds ordering of N-S,  $n = 2$ , steady subsonic BL**

DP<sub>y</sub>: pressure through BL is constant  
 $\Rightarrow P(x)$  from potential farfield DM solution

DP<sub>x</sub>:  $\partial^2 u / \partial x^2$  is  $O(\delta^2)$ , hence negligible,  $Re = O(\delta^{-2}) \gg 1$   
 $\Rightarrow$  BL DP<sub>x</sub> is initial-value on  $x \geq x_0$

DM:  $\partial v / \partial y = - \partial u / \partial x$ , hence initial value on  $0 \leq y < \delta(x)$

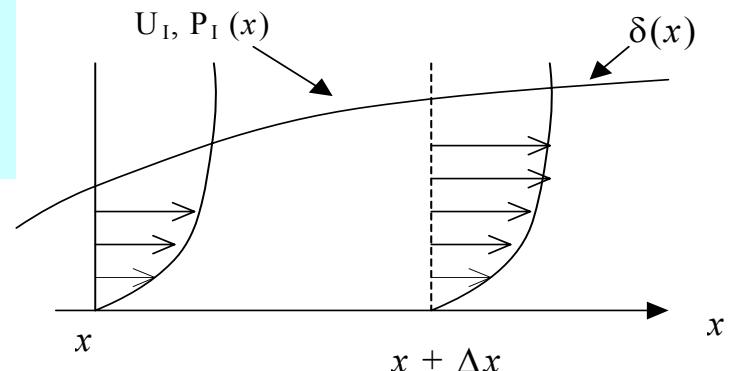
**Conservation principles for laminar BL flow simplify to**

$$\begin{aligned} L(u) &= u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + Eu \frac{dP_I}{dx} - \frac{1}{Re} \frac{\partial^2 u}{\partial y^2} = 0 \\ L(v) &= \frac{\partial v}{\partial y} + \frac{\partial u}{\partial x} = 0 \end{aligned}$$

BCs:  $u(x, y = 0) = 0 = v(x, y = 0)$

$$\left. \frac{\partial u}{\partial y} \right|_{x, y/\delta > 1} = 0$$

$$\delta(x) \equiv y(u(x) / U_I(x)) \equiv 0.99$$



# FM.11 Boundary Layer Flow, Turbulence

BL form of NS valid only for  $\text{Re} \gg 1$

aircraft	Mach	$U_\infty$ (m/s)	L (m)	Re	Re/L
commuter	0.3	125	10	3E07	$O(E06)$
wide body	0.9	250	40	2E08	$O(E06)$

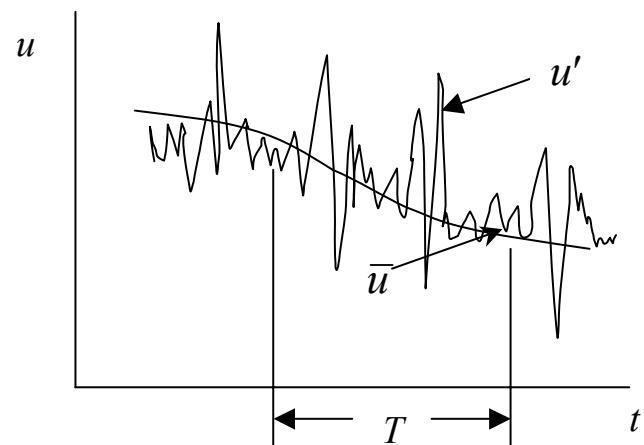
BL flows will be turbulent (!)

resolution of BL velocity components

$$u(\mathbf{x}, t) \equiv \bar{u}(\mathbf{x}) + u'(\mathbf{x}, t)$$

time-averaging

$$\bar{u}(\mathbf{x}) \equiv \lim_{T \rightarrow \infty} \frac{1}{T} \int_{t_0}^{t_0+T} u(\mathbf{x}, \tau) d\tau$$
$$\overline{u'} = 0$$



# FM.12 Boundary Layer Flow, Reynolds Stress

## Time averaging of BL DM and DP

DM: both terms linear, hence  $\nabla \cdot \bar{\mathbf{u}} = 0 = \nabla \cdot \mathbf{u}'$

DP<sub>x</sub>: non-linear convection term generates a new contribution

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \Rightarrow \frac{\partial}{\partial x} (\bar{u}\bar{u}) + \frac{\partial}{\partial y} (\bar{v}\bar{u}) \text{ via DM}$$

$$\bar{u}\bar{u} \Rightarrow \bar{u}\bar{u} + \bar{u}'\bar{u}'$$

$$\bar{v}\bar{u} \Rightarrow \bar{v}\bar{u} + \bar{v}'\bar{u}'$$

Reynolds ordering confirms that  $O(\bar{u}'\bar{u}') \approx O(\bar{v}'\bar{u}') \approx O(\delta)$

$$\frac{\partial}{\partial x} (\bar{u}\bar{u} + \bar{u}'\bar{u}') \Rightarrow O(1 \cdot 1 / 1 + \delta / 1)$$

$$\frac{\partial}{\partial y} (\bar{v}\bar{u} + \bar{v}'\bar{u}') \Rightarrow O(\delta \cdot 1 / \delta + \delta / \delta)$$

hence:

Reynolds normal stress  $\bar{u}'\bar{u}'$  contribution negligible

Reynolds shear stress  $\bar{v}'\bar{u}'$  contribution must be included

# FM.13 Boundary Layer Flow, Turbulence Modeling

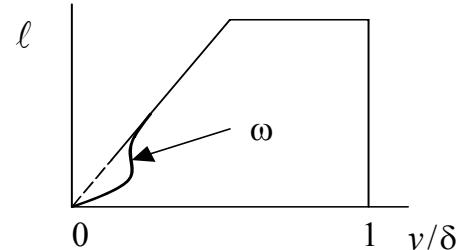
Reynolds kinematic shear stress modeled after Stokes, FM.2

$$\overline{v' u'} = -v^t \frac{\partial \bar{u}}{\partial y} \quad , \quad v^t \equiv \text{turbulent "eddy" viscosity, units are } L^2 / t$$

Prandtl mixing length model

$$v^t \equiv (\omega \ell)^2 \left| \frac{\partial \bar{u}}{\partial y} \right| \Rightarrow (L^2)(1/t)$$

where:  $\ell \equiv \text{mixing length}$   
 $\omega = \text{van Driest near wall damping}$



Turbulent kinetic energy-dissipation model

$$v^t \equiv C_\mu k^2 / \epsilon \Rightarrow (L/t)^4 (t^3 / L^2)$$

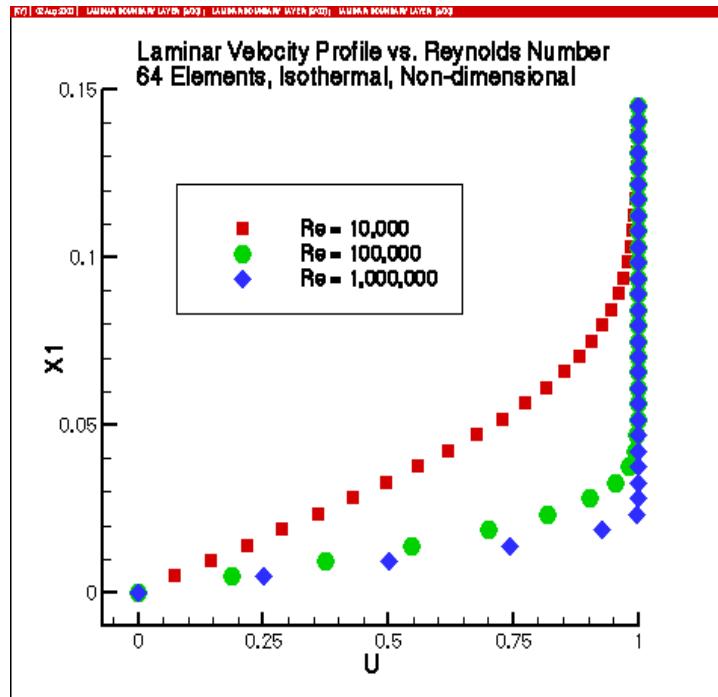
where:

$$k \equiv \frac{1}{2} \left( \overline{\mathbf{u}' \cdot \mathbf{u}'} \right) = \frac{1}{2} \left( \overline{u' u'} + \overline{v' v'} + \overline{w' w'} \right)$$
$$\epsilon \equiv \frac{2\nu}{3} \left( \frac{\partial u'_i}{\partial x_k} \frac{\partial u'_i}{\partial x_j} \right) \delta_{jk}$$

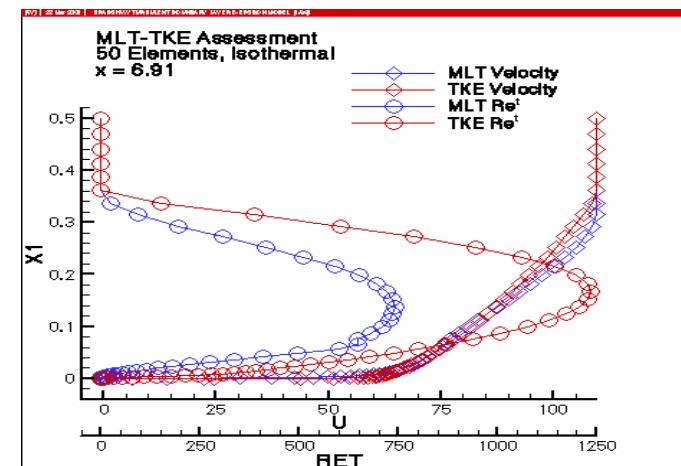
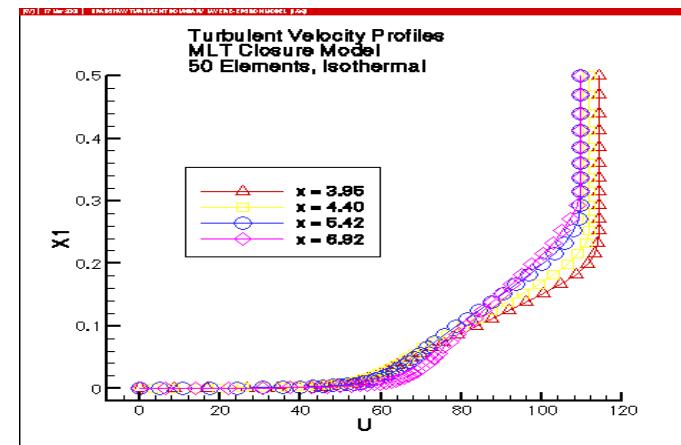
and:  $L(k)$  and  $L(\epsilon)$  BL forms augment BL DM & DP<sub>x</sub>

# FM.14 Aerodynamic Boundary Layers, Laminar & Turbulent

Downstream velocity profiles,  
laminar,  $10^4 \leq Re/L \leq 10^6$



Turbulent BL,  $Re/L \approx 10^5$



# FM.15 Navier-Stokes, Computational Fluid Dynamics

Fluid-thermal-structural system design uses “CFD”

for Reynolds-averaged, turbulent, unsteady incompressible flow

$$DM: \quad \nabla \cdot \mathbf{u} = 0$$

$$DP: \quad \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} + Eu \nabla p - \nabla \cdot (\text{Re}^{-1} + v^t) \nabla \mathbf{u} + \frac{Gr}{\text{Re}^2} \Theta \hat{\mathbf{g}} = \mathbf{0}$$

$$DE: \quad \frac{\partial \Theta}{\partial t} + \mathbf{u} \cdot \nabla \Theta - \text{Re}^{-1} \nabla \cdot (\text{Pr}^{-1} + v^t / \text{Pr}^t) \nabla \Theta + s_\Theta = 0$$

$$DE': \quad \frac{\partial k}{\partial t} + \mathbf{u} \cdot \nabla k - \text{Re}^{-1} \nabla \cdot (\text{Pr}^{-1} + v^t / \text{Pr}^t) \nabla k + \mathbf{T} \nabla \mathbf{u} - \varepsilon = 0$$

$$DE_m': \quad \frac{\partial \varepsilon}{\partial t} + \mathbf{u} \cdot \nabla \varepsilon - \text{Re}^{-1} \nabla \cdot (C_\varepsilon v^t / \text{Pr}^t) \nabla \varepsilon + C_\varepsilon^1 \mathbf{T}_k^\varepsilon \frac{\varepsilon}{k} \nabla \mathbf{u} - C_\varepsilon^2 \varepsilon^2 / k = 0$$

where:

non-D groups were defined on FM.4

turbulence closure, generalization of BL development, FM.12,  $v^t \equiv C_\mu k^2 / \varepsilon$

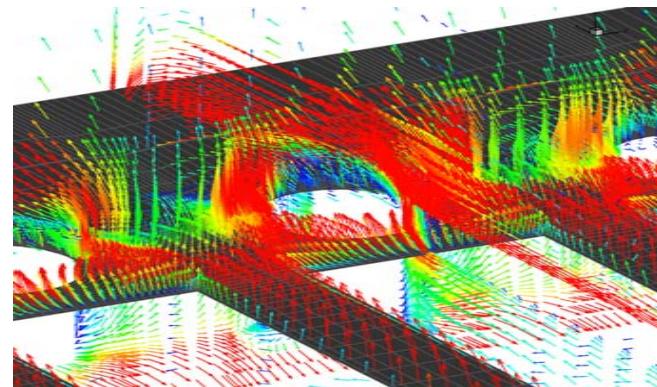
algebraic Reynold stress model

$$- \mathbf{T} = - \frac{2}{3} k \delta + v^t (\nabla \mathbf{u} + (\nabla \mathbf{u})^T) + \dots$$

# FM.16 Navier-Stokes, CFD, Algorithm Issues

## NS turbulent flow conservation law PDEs

initial-value  
explicitly non-linear!  
multiple DOF/node!  
as given, are ill-posed!  
intrinsically unstable for  $\text{Re} \gg 1$



## Commercial CFD codes contain required capabilities

have 15-20 year development history  
are based on FD, FV and/or FE discrete methods  
learning curve is *steep*!  
chances for error are numerous  
output interpretation requires color graphics & animations

# FM.17 Incompressible N-S, Well-Posedness

Consider unsteady isothermal laminar NS

DM:  $\nabla \cdot \mathbf{u} = 0$

DP:  $\mathbf{u}_t + \mathbf{u} \cdot \nabla \mathbf{u} + Eu \nabla p - Re^{-1} \nabla^2 \mathbf{u} = 0$   
 $\Rightarrow 4 \text{ PDEs on } \mathbf{u}, \text{ none on } p !$

Mathematically, DM is a *constraint* on solutions to DP

theories to enforce the constraint include

pseudo-compressibility:

$$DM \Rightarrow \beta^{-1} p_t + \nabla \cdot \mathbf{u} = 0$$

pressure projection:

$$\|\nabla \cdot \mathbf{u}^h\| \Rightarrow \varepsilon > 0, \text{ iteratively}$$

vector field theory:

$$DM \text{ guarantees } \mathbf{u} = \nabla \times \Psi$$

$\nabla \times \text{DP}$  eliminates pressure appearance

$\Rightarrow$  for  $n = 2$ , produces streamfunction-vorticity formulation

# FM.18 Streamfunction-Vorticity Navier-Stokes

For  $n = 2$ :  $\mathbf{u} = \nabla \times \psi \hat{\mathbf{k}}$  and  $\omega \equiv \nabla \times \mathbf{u} \cdot \hat{\mathbf{k}}$

DM:  $\nabla \cdot \mathbf{u} = \nabla \cdot \nabla \times \psi \hat{\mathbf{k}} = 0$  identically

$\hat{\mathbf{k}} \cdot \nabla \times \mathbf{D}\mathbf{P}$ :  $\omega_t + \nabla \times \psi \hat{\mathbf{k}} \cdot \nabla \omega - \text{Re}^{-1} \nabla^2 \omega = 0$

kinematics:  $\omega = \nabla \times \mathbf{u} \cdot \hat{\mathbf{k}} = \nabla \times \nabla \times \psi \hat{\mathbf{k}} \cdot \hat{\mathbf{k}} = -\nabla^2 \psi$

## Steady-state N-S PDEs + BCs:

$$\mathcal{L}(\omega) = -\text{Re}^{-1} \nabla^2 \omega + \nabla \times \psi \hat{\mathbf{k}} \cdot \nabla \omega = 0$$

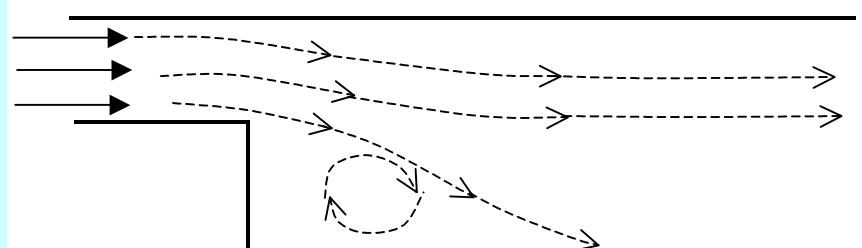
$$\mathcal{L}(\psi) = -\nabla^2 \psi - \omega = 0$$

$\partial\Omega_{\text{in}}$ :  $\mathbf{u}(y, x_{\text{in}}) \Rightarrow \omega_{\text{in}}, \psi_{\text{in}}$  via definitions

$\partial\Omega_{\text{out}}$ :  $\hat{\mathbf{n}} \cdot \nabla(\omega, \psi) = 0$

$\partial\Omega_{\text{wall}}$ :  $\psi = \psi_w = \text{constant}$

$$\hat{\mathbf{n}} \cdot \nabla \omega = f_w(\psi, \omega)$$



# FM.19 GWS<sup>h</sup>, Streamfunction-Vorticity NS, n = 2

## Galerkin weak statements:

for

$$q^N(x, y) \equiv \sum_{\alpha} \Psi_{\alpha}(\mathbf{x}) Q_{\alpha}, \quad q = \{\omega, \psi\}^T$$

$$\begin{aligned} \text{GWS}^N(\omega) &\equiv \int_{\Omega} \Psi_{\beta}(\mathbf{x}) \mathcal{L}(\omega^N) d\tau = \int_{\Omega} \Psi_{\beta} \left[ -\text{Re}^{-1} \nabla^2 \omega^N + \nabla \times \psi^N \hat{\mathbf{k}} \cdot \nabla \omega^N \right] d\tau \\ &= \int_{\Omega} \left[ \text{Re}^{-1} \nabla \Psi_{\beta} \cdot \nabla \Psi_{\alpha} \text{OMG}_{\alpha} + \Psi_{\beta} \nabla \times \Psi_{\gamma} \text{PSI}_{\gamma} \cdot \nabla \Psi_{\alpha} \text{OMG}_{\alpha} \right] d\tau + \text{BC} \\ \text{GWS}^N(\psi) &= \int_{\Omega} \Psi_{\beta} L(\psi^N) d\tau = \int_{\Omega} [\nabla \Psi_{\beta} \cdot \nabla \Psi_{\alpha} \text{PSI}_{\alpha} - \Psi_{\beta} \Psi_{\alpha} \text{OMG}_{\alpha}] d\tau + \text{BC} \end{aligned}$$

thus:

$$\text{GWS}^N \Rightarrow \text{GWS}^h = S_e \{ \text{WS} \}_e \equiv 0$$

$$\begin{aligned} \{ \text{WS}(\omega^h) \}_e &= \text{Re}^{-1} [\text{B2KK}]_e \{ \text{OMG} \}_e + \{ \text{PSI} \}_e^T [\text{B3K0K}]_e \{ \text{OMG} \}_e \\ &\quad + \text{Re}^{-1} [\text{A200}]_e \{ f_w(\psi^h, \omega^h) \}_e \end{aligned}$$

$$\{ \text{WS}(\psi^h) \}_e = [\text{B2KK}] \{ \text{PSI} \}_e - [\text{B200}]_e \{ \text{OMG} \}_e + [\text{A200}]_e \{ \text{U}_w \}_e$$

# FM.20 GWS<sup>h</sup> Details, Streamfunction-Vorticity NS

**GWS<sup>h</sup> for  $\omega^h$  involves  $\nabla \times \psi \hat{\mathbf{k}} \cdot \nabla \omega$**

$$\nabla \times \psi \hat{\mathbf{k}} \cdot \nabla \omega = \frac{\partial \psi}{\partial y} \frac{\partial \omega}{\partial x} - \frac{\partial \psi}{\partial x} \frac{\partial \omega}{\partial y}$$

$$\begin{aligned} \therefore [\text{B3K0K}]_e &= \int_{\Omega_e} \left[ \frac{\partial \{N\}}{\partial y} \{N\} \frac{\partial \{N\}^T}{\partial x} - \frac{\partial \{N\}}{\partial x} \{N\} \frac{\partial \{N\}^T}{\partial x} \right] dx dy \\ &\Rightarrow [\text{B3Y0X}]_e - [\text{B3X0Y}]_e \end{aligned}$$

**Vorticity Robin BC generated via TS on  $\partial \Omega^h$ :**

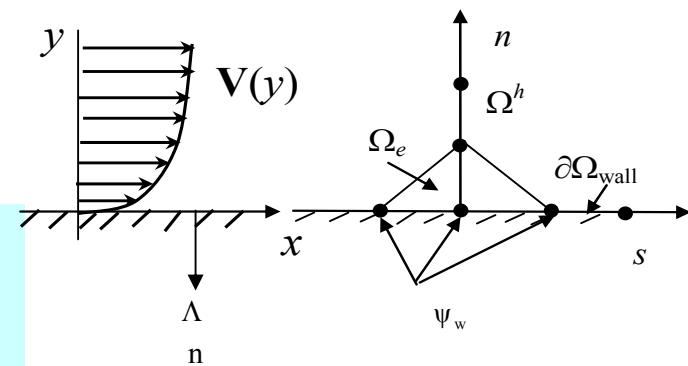
$$-\nabla^2 \psi - \omega = \frac{-\partial^2 \psi}{\partial s^2} - \frac{\partial^2 \psi}{\partial n^2} - \omega = 0 \Rightarrow \frac{d^2 \psi}{dn^2} = -\omega \quad \Big|_{\partial \Omega_{\text{wall}}}$$

**TS:**

$$\begin{aligned} \psi(\Delta n) &= \psi_w + \frac{d\psi}{dn} \Big|_w \Delta n + \frac{d^2 \psi}{dn^2} \Big|_w \frac{\Delta n^2}{2} + \frac{d^3 \psi}{dn^3} \Big|_w \frac{\Delta n^3}{6} + O(\Delta n^4) \\ &= \psi_w + U_w \Delta n - \omega_w \Delta n^2 / 2 - (d\omega/dn)_w \Delta n^3 / 6 \end{aligned}$$

**BC:**

$$\ell(\omega) = \hat{\mathbf{n}} \cdot \nabla \omega - (3/\Delta n) \omega + (6/\Delta n^2) (U_w) - (6/\Delta n^3) (\psi_{w+1} - \psi_w) = 0$$



# FM.21 Newton $\{\mathbf{F}\mathcal{Q}\}_e$ Template, $(\omega^h, \psi^h)$ $\mathbf{GWS}^h$

$\mathbf{GWS}^h \Rightarrow$  global Newton statement

$$[\text{Jacobian}] \{\delta Q\}^{p+1} = -\{\mathbf{F}\mathcal{Q}\}^p \Leftrightarrow S_e([\text{JAC}]_e) \{\delta Q\}^{p+1} = -S_e(\{\mathbf{F}\mathcal{Q}\}_e)$$

Template pseudo code for  $\{\mathbf{F}\mathcal{Q}\}_e$

$$\{\text{WS}(\cdot)\}_e \equiv (\text{const}) (\text{avg})_e \{\text{dist}\}_e (\text{metric}; \det)_e [\text{matrix}] \{Q \text{ or data}\}_e$$

$$\begin{aligned} \{\text{FOMG}\}_e &= (\text{Re}^{-1})(\cdot)(\cdot)(-1)[\text{B2KK}] \{\text{OMG}\} \\ &+ (\cdot)(\cdot) \{\text{PSI}\} (-1)[\text{B3K0K}] \{\text{OMG}\} \\ &+ (-3/\Delta n, \text{Re}^{-1})(\cdot)(\cdot)(1)[\text{A200}] \{\text{OMG} - f(\mathbf{U}, \Delta \psi)\} \end{aligned}$$

$$\begin{aligned} \{\text{FPSI}\}_e &= (\cdot)(\cdot)(\cdot)(-1)[\text{B2KK}] \{\text{PSI}\} \\ &+ (-1)(\cdot)(\cdot)(1)[\text{B200}] \{\text{OMG}\} \\ &+ (\cdot)(\cdot)(\cdot)(1)[\text{A200}] \{\mathbf{U}\} \end{aligned}$$

# FM.22 Newton Jacobian Template, $(\omega^h, \psi^h)$ GWS<sup>h</sup>

Newton jacobian formed via differentiation

$$[\text{JAC}]_e \equiv \frac{\partial \{FQ\}_e}{\partial \{Q\}_e} = \begin{bmatrix} [J\Omega\Omega] & [J\Omega\psi] \\ [J\psi\Omega] & [J\psi\psi] \end{bmatrix}_e$$

Jacobian template pseudo-code

$$[J\Omega\Omega]_e \equiv \frac{\partial \{FOMG\}_e}{\partial \{OMG\}_e} = (Re^{-1})(\ )\{ \ }(-1)[B2KK][ ] + (\ )( \ )\{PSI\}(-1)[B3K0K][ ] - (3/\Delta n, Re^{-1})(\ )\{ \ }(1)[A200][ ]$$

$$[J\Omega\psi]_e \equiv \frac{\partial \{FOMG\}_e}{\partial \{PSI\}_e} = (\ )( \ )\{OMG\}(-1)[B3K0KT][ ] - (6/\Delta n^3, Re^{-1})(\ )\{ \ }(1)[A200][\Delta PSIwall]$$

$$[J\psi\Omega]_e \equiv \frac{\partial \{FPSI\}_e}{\partial \{OMG\}_e} = (-1)(\ )\{ \ }(1)[B200][ ]$$

$$[J\psi\psi]_e \equiv \frac{\partial \{FPSI\}_e}{\partial \{PSI\}_e} = (\ )( \ )\{ \ }(-1)[B2KK][ ]$$

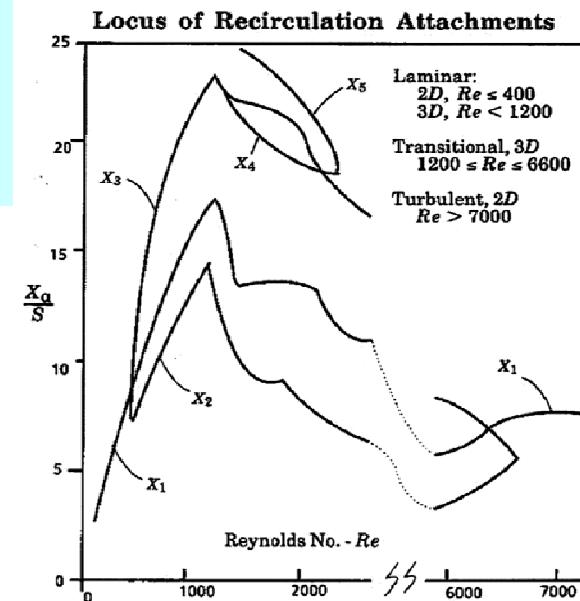
# FM.23 Incompressible N-S, Step Wall Diffuser

GWS<sup>h</sup> + Newton  $\Rightarrow$  computable matrix statement

$$S_e \begin{Bmatrix} J\Omega \Omega & J\Omega \psi \\ J\psi \Omega & J\psi \psi \end{Bmatrix}_e \begin{Bmatrix} \delta \text{OMG} \\ \delta \text{PSI} \end{Bmatrix}_e^{p+1} = - \begin{Bmatrix} \text{FOMG} \\ \text{FPSI} \end{Bmatrix}_e^p$$

## Step-well diffuser problem statement

primary separated flow region  
caused by step change in  $A(x)$   
reattachment  $x_1(\psi_w) = f(\text{Re})$   
multiple auxiliary separations in 3-D



## Computer lab design problem

determine  $x_1/S$  of dividing  $\Psi_1$  as  $f(\text{Re})$   
for  $100 \leq \text{Re} \leq 600$

